

AGU Fall Meeting - *San Francisco, 14-18 December 2015*

H42A-01 COMPLEXITIES OF FLOW AND TRANSPORT IN
POROUS MEDIA ACROSS DIVERSE DISCIPLINES III

Gravity-driven flow of non-Newtonian fluids
in heterogeneous porous media: a theoretical
and experimental analysis

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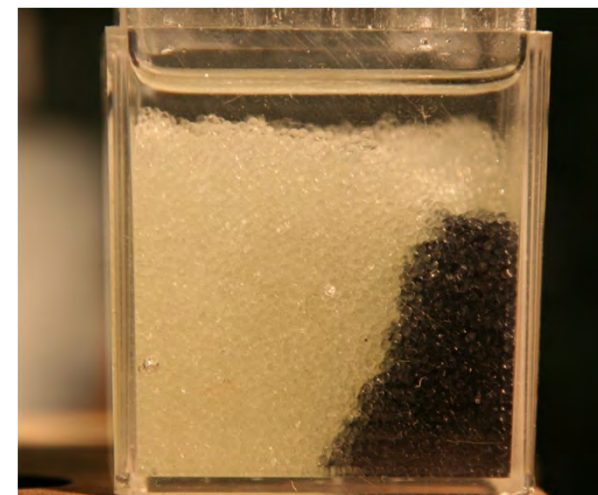
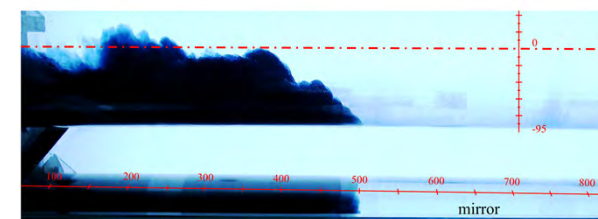
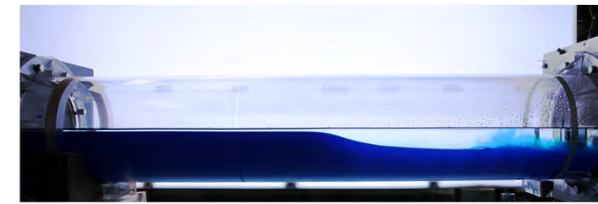
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Motivation (I)

“Gravity current” (GC): one fluid moves in horizontal direction into another fluid because the densities are different.

The pressure/buoyancy driving is “balanced” by either inertial, or viscous, adjustment of the fluid.



Viscous GC in porous media (PM) occur in many environmental processes:

- enhanced oil and heat recovery
- groundwater remediation
- carbon dioxide sequestration
- saltwater intrusion



Motivation (II)

In PM flow, fluid rheology is often non-Newtonian (NN):

- polymeric suspensions in enhanced oil recovery
- pollutants in environmental modelling
- muds in well drilling
- crude oil in reservoir engineering
- fluid carriers for nanoparticles in soil remediation
- injectable biomaterials in biological applications (orthopaedics, dental)



Need of efficient tools for understanding and prediction of NN gravity currents in PM



simplified (analytical) models provide reliable guidelines



experimental verification



Background and objective

- Analytical and numerical solutions (with experimental verification) are available in the literature for Newtonian GC in homogeneous PM (Huppert 2006, Ungarish 2009); reference cases: plane (Huppert and Woods 1995) and radial (Lyle et al. 2005) geometry
- Solutions for thin currents ($H/L \ll 1$) are self-similar (intermediate asymptotics)
- Solutions for flow of non-Newtonian power-law fluids were recently derived (Di Federico et al., *JNNFM* 2012a,b) and experimentally verified (Longo et al., *JFM* 2013) for plane/radial case
- Natural PM are inherently heterogeneous. Spatial heterogeneity affects GC spreading rate and extent and shape of porous domain invaded/reached

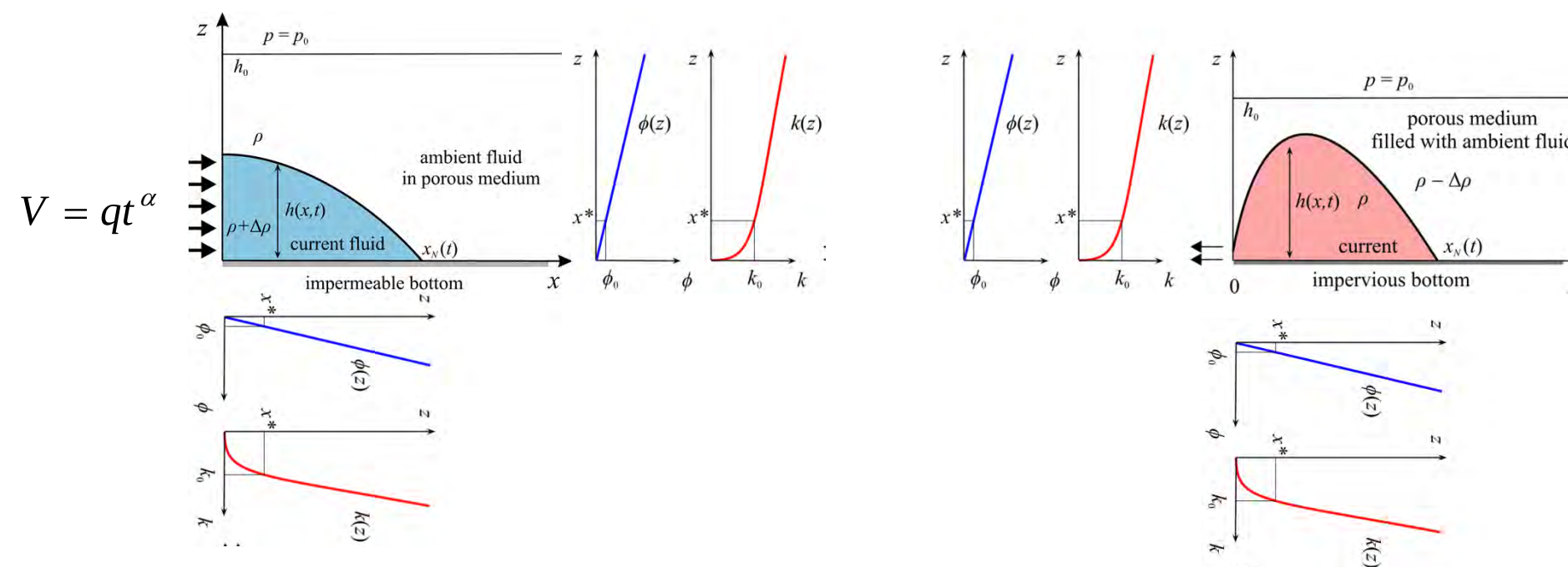


Need to explore the combined effect of rheology and heterogeneity considering non-Newtonian flow in media with variable properties



Scenarios

- Geometry: 2-D plane flow
- Fluid rheology: power-law fluid
- Spatial heterogeneity: permeability/porosity varying transverse or parallel to flow direction
- Type of release: instantaneous injection of constant mass, continuous injection, instantaneous injection of mound draining freely out of formation (dipole flow)





Flow law in PM

Stress-shear rate relationship, Ostwald–deWaele fluid,
simple shear

$$\tau = \tilde{\mu} |\dot{\gamma}|^{n-1} \dot{\gamma} = \mu_{app} \dot{\gamma}$$

$\tilde{\mu}$ consistency index [ML⁻¹Tⁿ⁻²]

n flow behavior index
 $n < 1$ shear-thinning (pseudoplastic)
 $n = 1$ Newtonian ($\mu_{app} \rightarrow \mu$)
 $n > 1$ shear-thickening (dilatant)

Eq. of motion for power-law
fluids in porous media
(e.g. Shenoy, 1995)

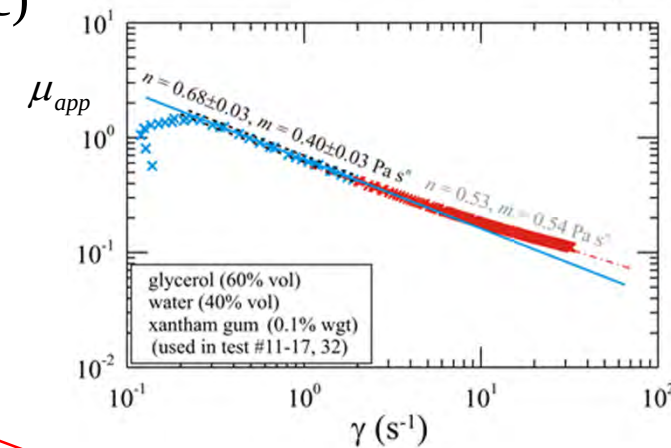
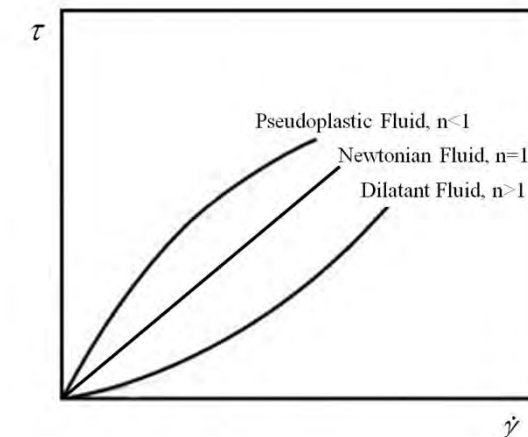
p pressure

$\mathbf{v}$ seepage flux

k permeability [L²]

ϕ porosity

$C_t = C_t(n)$ tortuosity



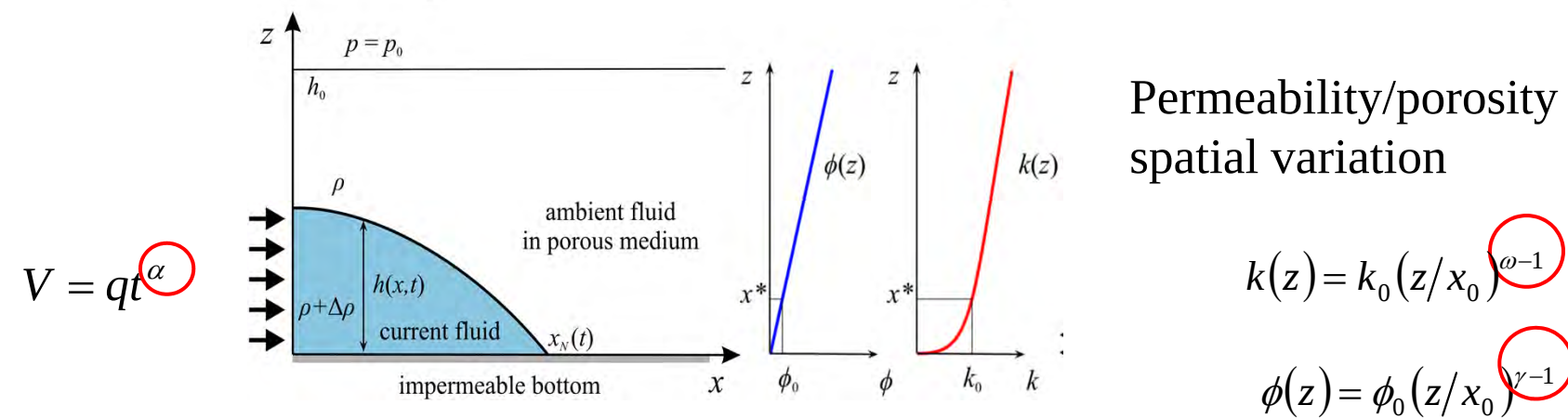
$$\nabla(p + \rho g z) = - \frac{1}{\Lambda k^{(1+n)/2}} |\mathbf{v}|^{n-1} \mathbf{v},$$

$$\Lambda \equiv \Lambda(\phi, \tilde{\mu}, n) = \frac{1}{2C_t} \left(\frac{50}{3} \right)^{(n+1)/2} \left(\frac{n}{3n+1} \right)^n \frac{\phi^{(n-1)/2}}{\tilde{\mu}}$$



Problem formulation

- i) immiscible displacement; ii) thin intruding current; iii) no motion of ambient fluid
- iv) no capillary effects; v) instantaneous/continuous injection



Flow law

$$u_x = (\Lambda \Delta \rho g)^{1/n} k^{(1+n)/2n} \left(-\frac{\partial h}{\partial x} \right)^{1/n}$$

Mass balance

$$\frac{\partial}{\partial x} \int_0^h u dz + \frac{\partial}{\partial t} \int_0^h \phi dz = 0$$

Condition at the current tip

$$h(x_N(t), t) = 0$$

Global mass balance

$$\int_0^{x_N(t)} \int_0^h \phi dz dx = qt^\alpha$$

$\alpha=0$ constant volume
 $\alpha=1$ constant inflow rate



Self-similar solution

Dimensionless coordinates

$\boxed{\text{PDE}}$ $\eta = F_1^{F_4} x/t^{F_2}$ Similarity Variable $\eta_N = \eta(x_N)$ $\zeta = \eta/\eta_N \in [0,1]$
 $x_N(t) = (\eta_N/F_1^{F_4})t^{F_2}$ Current tip position $F_i = F_i(\alpha, n, \gamma, \omega), i = 1, \dots, 5$ Numerical factors
 $h(x, t) = F_1^{F_4/\gamma} \eta_N^{F_5/\gamma} t^{F_3} \Phi(\zeta)$ Current height $\Phi(\zeta)$ Shape function

—————→ $\boxed{\text{ODE}}$

$$\frac{d}{d\zeta} \left[\Phi^{F_1} \left(-\frac{d\Phi}{d\zeta} \right)^{1/n} \right] + F_2 \zeta \Phi^{\gamma-1} \frac{d\Phi}{d\zeta} - F_3 \Phi^\gamma = 0 \quad \eta_N = \left(\int_0^1 \Phi^\gamma d\zeta \right)^{-1/(F_5+1)} \quad \Psi(1) = 0$$

Closed-form solution for $\alpha=0$, numerical for $\alpha>0$

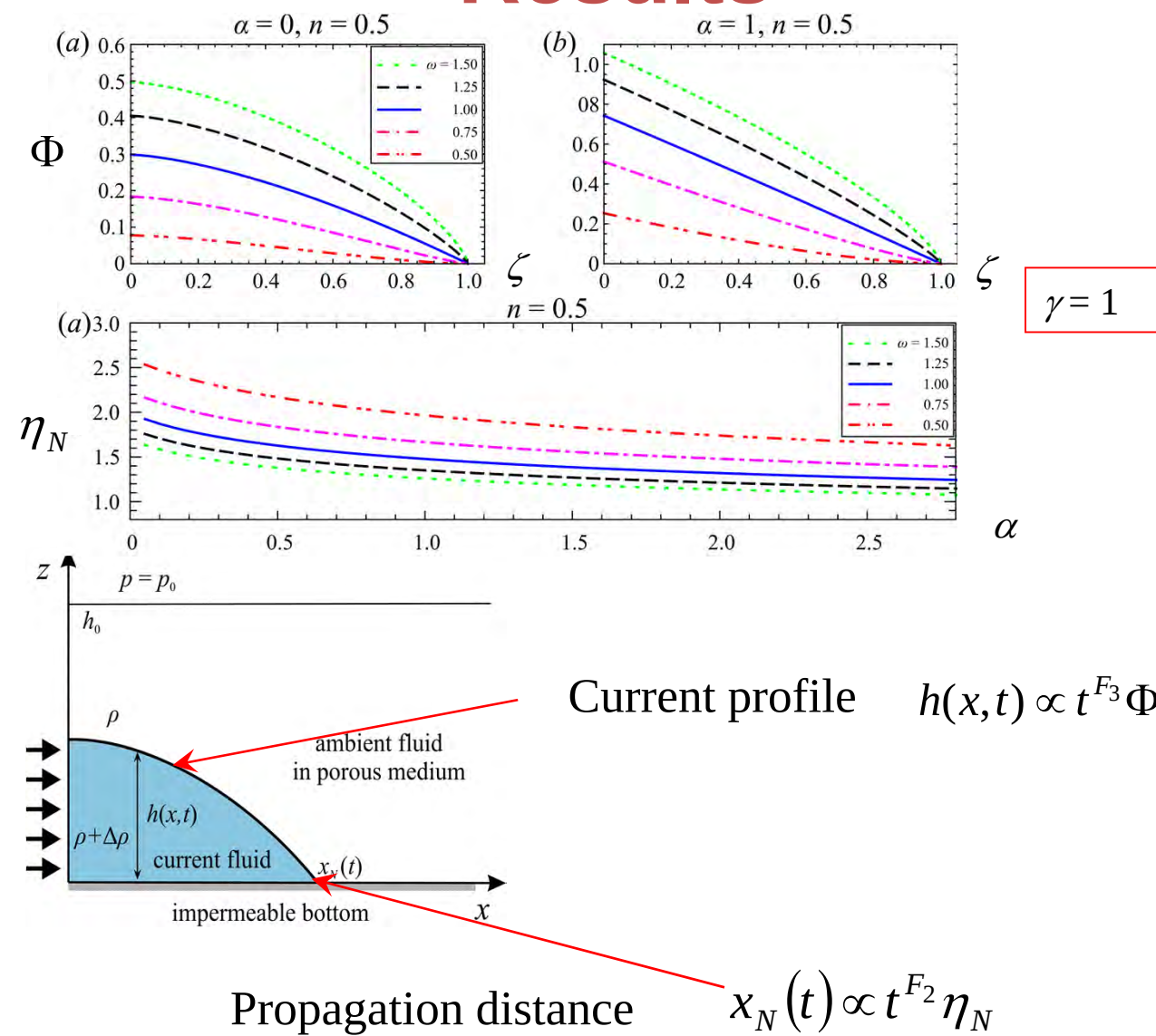


$$\Psi(\zeta) = \left(\frac{F_{20}^n}{F_5 \gamma^{n-1}} \right)^{F_5/[\gamma(n+1)]} (1 - \zeta^{n+1})^{F_5/[\gamma(n+1)]}; \eta_N = \left[\frac{1}{\gamma} \left(\frac{F_{20}^n}{F_5 \gamma^{n-1}} \right)^{F_5/[\gamma(n+1)]} \frac{F_5}{(F_5+1)(n+1)} B\left(\frac{1}{n+1}, \frac{F_5}{n+1} \right) \right]^{-1/F_5+1}$$

$F_{20} = F_2(\alpha=0)$

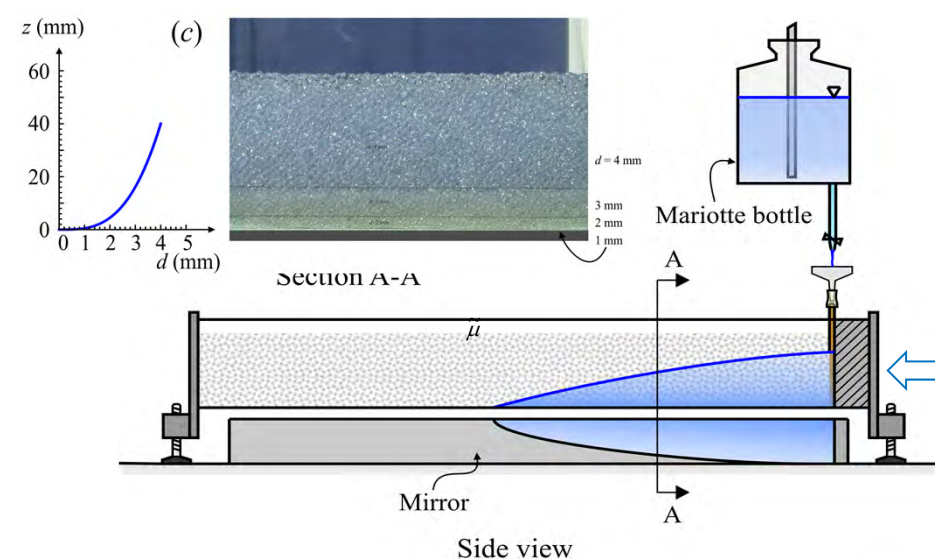


Results





Experimental setup (I)

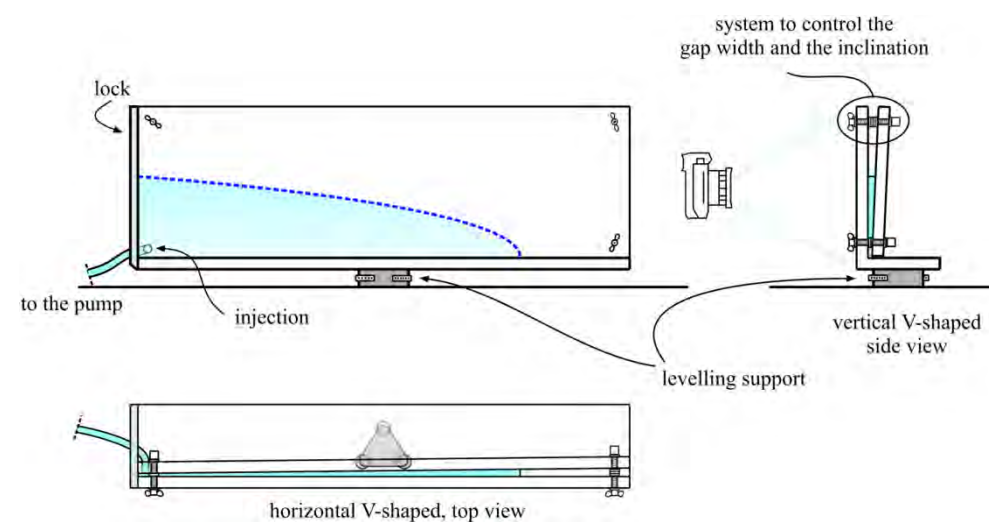


Direct simulation

- Porous medium=glass ballotini
- Vertical heterogeneity (k) reproduced via different strata with different diameter and thickness

Analogue simulation

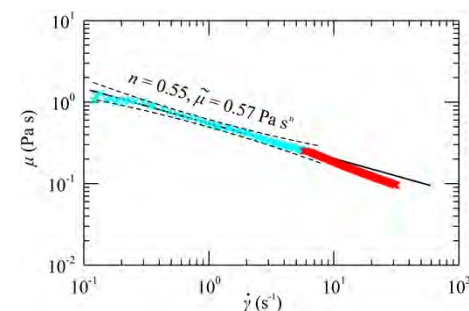
- Hele-Shaw analogy formally developed for NN flow
- Vertical/horizontal heterogeneity (k and ϕ) reproduced via cell with variable aperture in horizontal/vertical direction





Experimental setup (II)

- Different power-law fluids (mix Glycerol, water and Xanthan gum)
- Fluid rheological parameters determined a priori via rheometer
- Two high-resolution photocameras employed to record current tip and profile
- Constant inflow rate Q ($\alpha = 1$)
- Horizontal (A) and vertical (B) variation of properties



A

#	β	δ	b_0	$\tilde{\mu}$ (Pa s ⁿ)	n	ρ (kg m ⁻³)	q (ml s ⁻¹)
6	3	1	0.00205	0.34	0.47	1193	0.609
7 ^a	3	1	0.00308	0.34	0.47	1193	0.600
8	3	1	0.00308	0.34	0.47	1193	0.317
10	3	1	0.00308	0.20	0.45	1100	0.580
11	3	1	0.00308	0.20	0.45	1100	1.59
12	3	1	0.00304	0.20	0.45	1100	1.37

B

#	ω	γ	b_0	μ (Pa s ⁿ)	n	ρ (kg m ⁻³)	q (ml s ⁻¹)
1	4	2	0.00469	0.10	1	1230	0.639
2	4	2	0.00469	0.34	0.47	1193	0.296
3	4	2	0.00469	0.34	0.47	1193	0.233
13	4	2	0.00469	0.20	0.45	1100	2.05
14	4	2	0.00469	0.20	0.45	1100	2.28
15	4	2	0.00469	0.20	0.45	1100	0.27
19	4	2	0.09800	0.34	0.47	1193	0.23
20 ^a	4	2	0.01348	0.34	0.47	1193	0.28
9	1.63	1	-	0.34	0.47	1193	20.46
16	1.63	1	-	0.2	0.45	1100	81.33
17	1.63	1	-	0.2	0.45	1100	18.6
18 ^a	1.63	1	-	0.34	0.47	1193	8.65



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2D non-Newtonian power-law fluid flow in vertical varying permeability

Test 18

$\alpha = 1.0$ $d = 1 - 4$ mm, $\omega = 1.63$, $Q = 8.65$ ml/s/m

$n = 0.47$, $m = 0.34$ Pa sⁿ, $\rho = 1193$ kg/m³



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28th October 2014



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2D non-Newtonian power-law fluid flow in vertically increasing permeability and porosity

Test 20

$\alpha = 1.0$, $\omega = 4$, $\gamma = 2$, $Q = 0.280$ ml/s

$n = 0.47$, $m = 0.34$ Pa sⁿ, $\rho = 1193$ kg/m³



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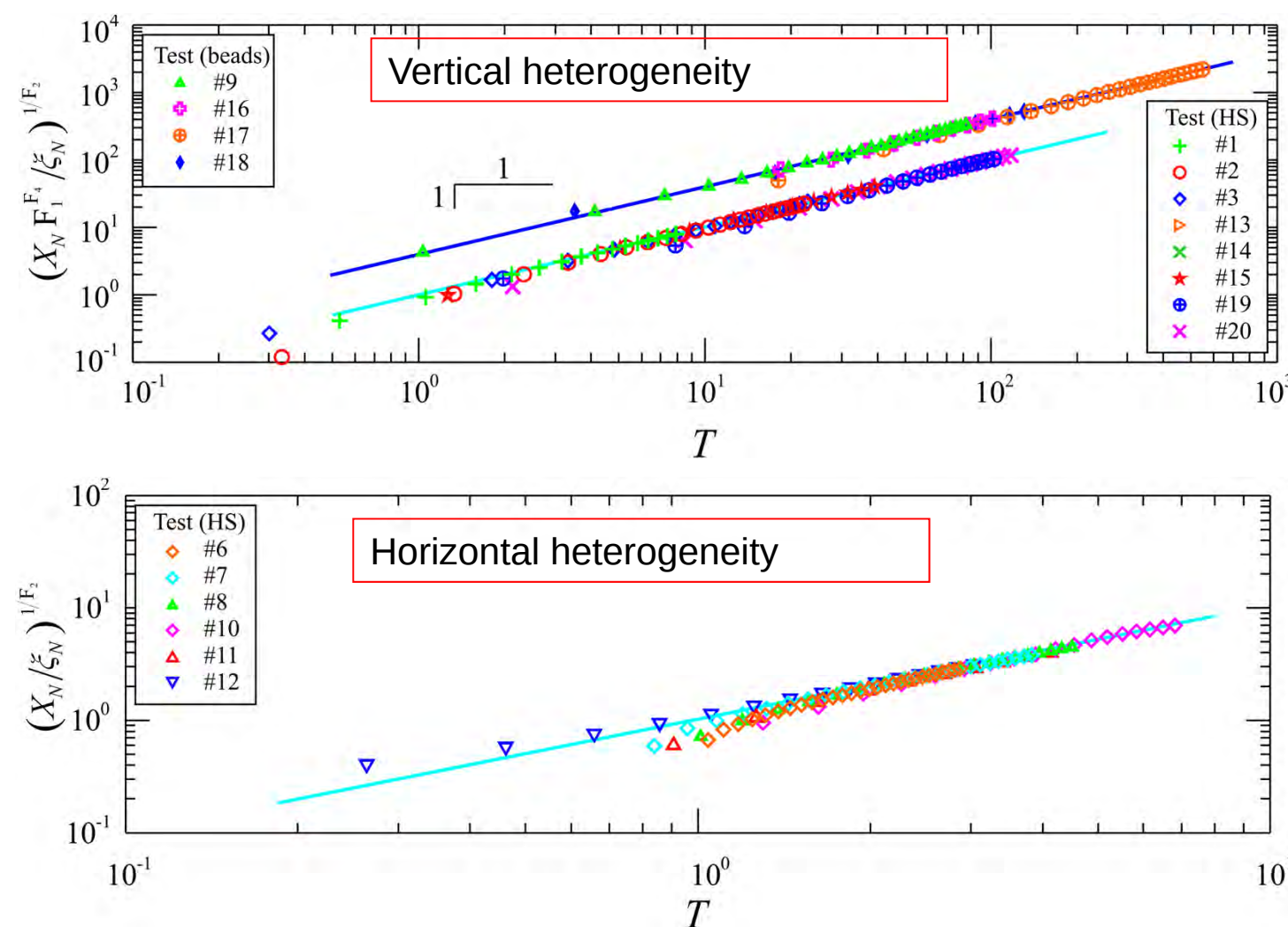
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31th October 2014



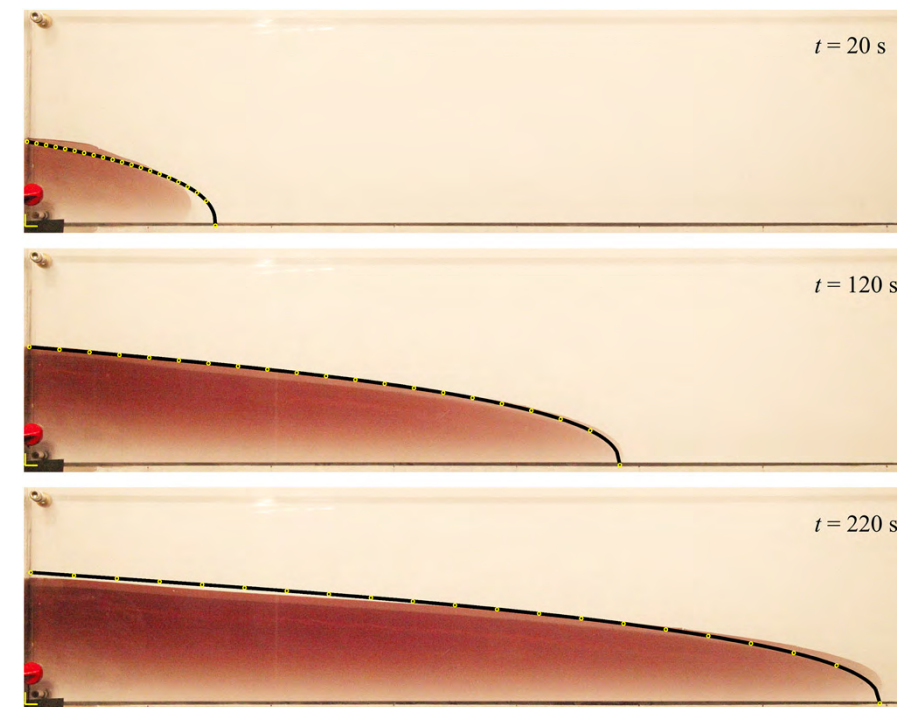
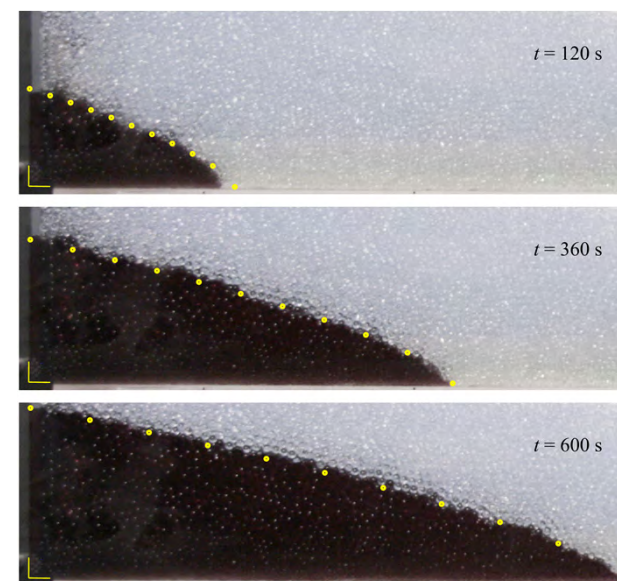
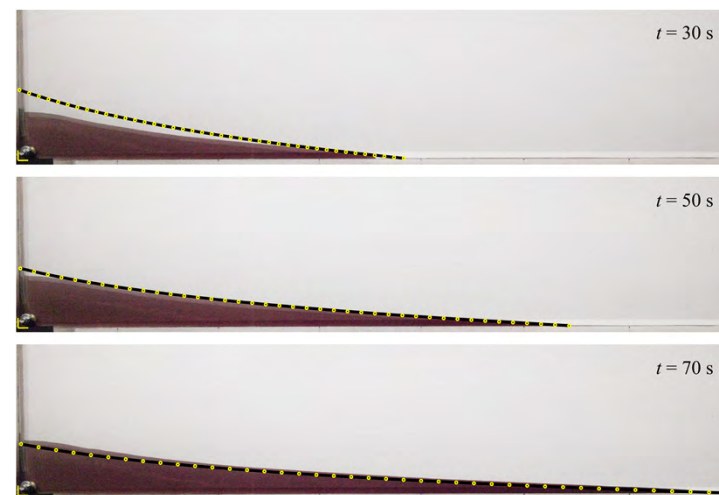
Comparison with theory: front



- Scaled non-dimensional position of the front end x_N against time
- Experimental results agree with theory, some discrepancy at early times



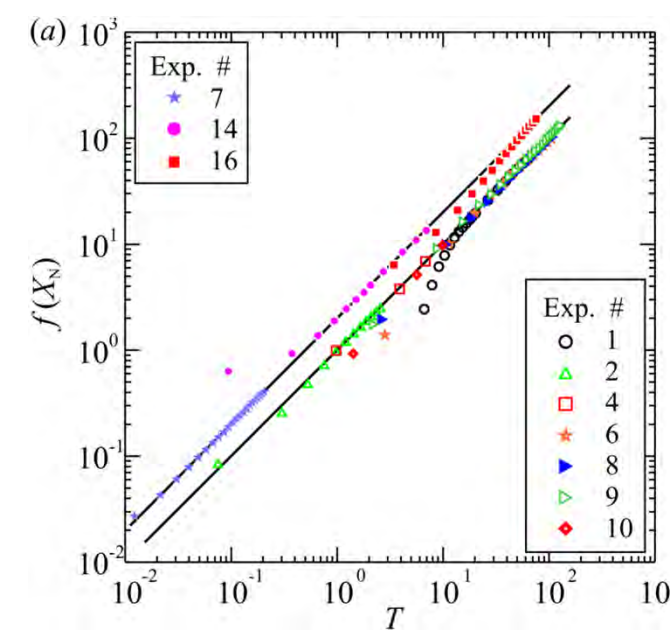
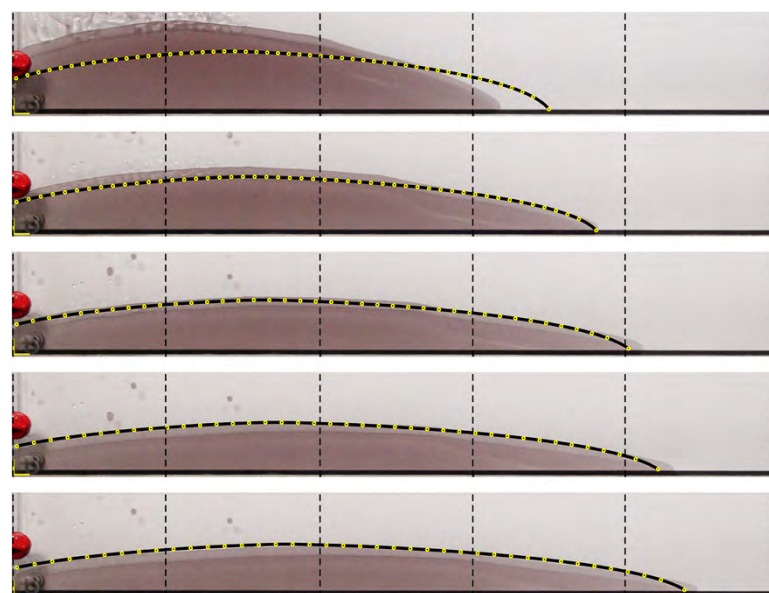
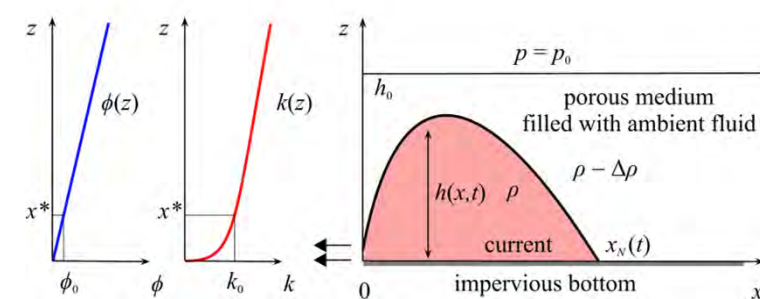
Comparison with theory: profile



- Current profiles at different times
- Agreement fairly good, with discrepancies near the origin / at early time



Dipole flow





Conclusions

- Propagation of thin GC of power-law fluids in PM amenable to similarity solution for variety of scenarios (geometry, fluid, spatial heterogeneity, release rate, ...)
- Earlier results generalized (fluid, spatial heterogeneity)
- Current front/profile controlled by model parameters (α , n , γ , ω)
- Theory supported by experiments with PM simulation: i) direct ii) Hele-Shaw analogue, with different permeabilities, flow rates, and fluids
- Hele-Shaw analogy for NN flow in spatially heterogeneous PM formally developed
- Ongoing developments:
 - Confined NN flow in spatially heterogeneous PM
 - Stochastic heterogeneity